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Synthesis of polyamide 6/nano-hydroxyapatite hybrid (PA6/n-HAp) for the sorption of rare earth elements and uranium

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ABSTRACT

Polyamide (PA6) and hydroxyapatite (n-HAp) have intrinsic sorption properties for metal ions. Their association by melt compounding allows manufacturing a composite material (PA6/n-HAp) efficient for the binding of uranyl and rare earth metal ions (REEs) in acidic solution (in the pH range 2–2.5). The composite shows enhanced sorption capacities (5–7 times) compared with single PA6 material. The structuration of the material slightly improves textural properties but contributes to improve the accessibility and availability of reactive groups (including by size distribution). Metal sorption proceeds mainly through complexation of amide reactive groups as shown by FTIR characterization (modification of the environment of C=O and NH groups) rather than ion-exchange/electrostatic attraction. Maximum sorption capacities approach 0.34 mmol U g⁻¹, 0.49 mmol Er g⁻¹ and 0.70 mmol Nd g⁻¹: the preference may be correlated to the covalent rather than ionic character of these metal ions. Uptake kinetics are relatively slow (requiring up to 6–8 h, under selected experimental conditions): the textural properties of the composite (pore size: 2.6 nm) limit the mass transfer properties (though slightly enhanced compared with PA6 precursor). The resistance to intraparticle diffusion constitutes the major controlling step for uptake kinetics. Nitric acid is the most efficient eluent for the desorption of loaded metals (efficiency exceeds 94 %); noticeably U(VI) elution is optimal at 1 M HNO₃ concentration, contrary to REEs that require lower concentration (i.e., 0.1 M). Preliminary tests on sulfuric acid leachates of Egyptian ores demonstrate that the sorbent maintains good sorption properties for REEs and U despite the complexity of the solution. The sorbent has a marked preference for REEs, U and Th against base and alkali metals.

Keywords:

Polyamide

Nano hydroxyapatite

Composite sorbent

Uranyl and rare earth

Uptake kinetics

Sorption isotherms and desorption efficiency

Material characterization

1. Introduction

The removal of metal ions from contaminated water streams is an important challenge for industry because of the strengthening of governmental and international regulations, the demand of communities for better environmental protection, and the potential health effects associated with hazardous metal bioaccumulation. The recycling of valuable metals such as rare earth elements and the valorization of low-grade resources (industrial wastes, sub-products, and marginal ores) are also of critical importance for the provisional supply of high-tech industries and nuclear power industry (uranium) [1,2]. Many resources simultaneously contain rare earths and uranium, especially in Egyptian mining areas. It is thus important designing processes that can

contribute to the removal and valorization of these strategic metals from acid leachates. Indeed, leaching methods remain the most used techniques for the extraction (solid->liquid transfer) of metals from low-grade ores. In the liquid phase, the metals may be recovered by precipitation [3], mineral sorbents [4–8], agricultural wastes [9], functionalized composites [10,11], solvent extraction [1,12], activated carbon [13] or carbonized biomass [14], membrane processes [15], impregnated resin [16] or ion-exchange and chelating resins [17–22], depending on the composition of the leachates, the concentration of metals, and the flux of the effluent. Usually, sorption processes are preferred for the treatment of dilute solutions. Many reactive groups have shown affinity for rare earth and uranium including amidoxime [23–26], sulfonic and phosphonic groups [21,27–31].

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Polyamide-based materials [32–34] and soluble eggshell membrane protein-based nanocomposites adsorbents [35,36] have been successfully tested for the recovery of metal ions, including uranium [15,37] and rare earths [38]. However, the sorption capacities were usually low (in the range 0.5–0.62 mmol g⁻¹ for Er(III), Tb(III) and Dy(III)) with optimum sorption close to pH 5, or about 0.08 mmol U g⁻¹ at pH 7 [39]. These materials have been also frequently designed as composite by incorporation of silica [40], clays [41,42], carbon [43] or biomass [44] to (a) improve specific surface area, (b) change hydrophilic/hydrophobic characteristics and (c) enhance sorption performance. The functionalization of polyamide-based materials has been also used for improving metal sorption [45–48].

Hydroxyapatite (HAp) is part of the mineral sorbents that were tested for metal sorption [39,49–54]. Porous hydroxyapatite binds up to 0.47 mmol U g⁻¹ [49]. For Nd(III) and Sm(III), sorption capacities as high as 2.24 mmol Nd g⁻¹ and 2.46 mmol Sm g⁻¹ were reported for nano-hydroxyapatite (n-HAp) [52]. Managing nanoparticles for the treatment of large water streams require complex solid/liquid separation; therefore, n-HAp is frequently associated to supports that improve the reactivity and the readily solid/liquid separation (surface deposition [55]; incorporation of magnetic particles [51,52], functionalization [56] etc.).

Composites associating polyamide and n-HAp have been previously designed for biological application [57–60]. These composite materials are usually manufactured by melt-compounding [58,61]. The literature on the application of this type of material for metal sorption is scarce. The objective of the current work precisely consists of evaluating the effect of the incorporation of n-HAp in polyamide 6 (PA6) on the sorption of U(VI), Nd(III) (as a representative of light rare earth elements, LREE) and Er(III) (heavy rare earth, HREE) from tri-component solutions. A special attention is paid to the recovery of these metals from acidic solutions because most of the leachates produced in the treatment of uranium ores are acidic. Therefore, the sorption performances for U(VI) and REE(III)s are compared for raw PA6 sorbent and PA6/n-HAp composite through (a) the study of the effect of pH, sorbent dosage, and (b) the investigation of uptake kinetics, sorption isotherms, and metal desorption (selection of type and concentration of eluent). This comparison will help highlighting the beneficial effect of the incorporation of the mineral compound on the availability and accessibility of reactive groups (measured through the comparison of sorption isotherms and uptake kinetics) and the possible synergies of PA6 and n-HAp. The physical and chemical properties are characterized through SEM, TEM (for n-HAp) observation, EDX, XRD, TGA, BET and FTIR spectroscopy analysis, and zetametry measurements, with the objective of identifying the sorption mechanisms involved in metal binding and the limiting steps in the transfer of target metals. The last part of the work consists of the use of the composite PA6/n-HAp sorbent for the treatment of an acidic leachate of local Egyptian ores (from El Sella mining area).

2. Materials and methods

2.1. Materials

Calcium nitrate tetrahydrate, Ca(NO₃)₂·4H₂O (99 %) and ammonium hydroxide solution, NH₄OH (25 % NH₃) were supplied by Sigma Aldrich Chemie GmbH (Taufkirchen, Germany). Ammonium phosphate trihydrate, (NH₄)₃PO₄·3H₂O (99 %) was purchased from CHEMOS GmbH & Co. KG (Aldorf, Germany). Polyamide 6 (PA6) powder was purchased from Sigma Aldrich Chemie GmbH (Taufkirchen, Germany).

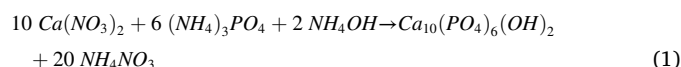
Depleted uranyl nitrate solution (10 g L⁻¹ stock solution, SPEX CertiPrep) was purchased from Fisher Scientific SAS (Illkirch-Graffenstaden, France). Erbium chloride (ErCl₃) and neodymium chloride (NdCl₃) were supplied by Sigma-Aldrich (Saint-Quentin-Fallavier, France). Nitric, hydrochloric, and sulfuric acids (analytical grade), used for desorption tests, were supplied by Sigma-Aldrich (Saint-Louis, MO,

USA).

2.2. Synthesis of sorbent (PA6/n-HAp)

2.2.1. Synthesis of n-hydroxyapatite (n-HAp)

The wet method was used for preparing n-HAp nanoparticles. Calcium nitrate (0.2 M – 50 mL) was slowly dropped into the ammonium phosphate solution (0.12 M – 50 mL) under vigorous stirring (900 rpm) at 80 °C for 4 h using a MS300 hot plate magnetic stirrer (Shanghai Leewen Scientific Instrument Co., Ltd, Shanghai, China). The pH was kept constant (in the range 10–12) using ammonium hydroxide solution (25 %, v/v). The synthesis procedure can be described by the equation:



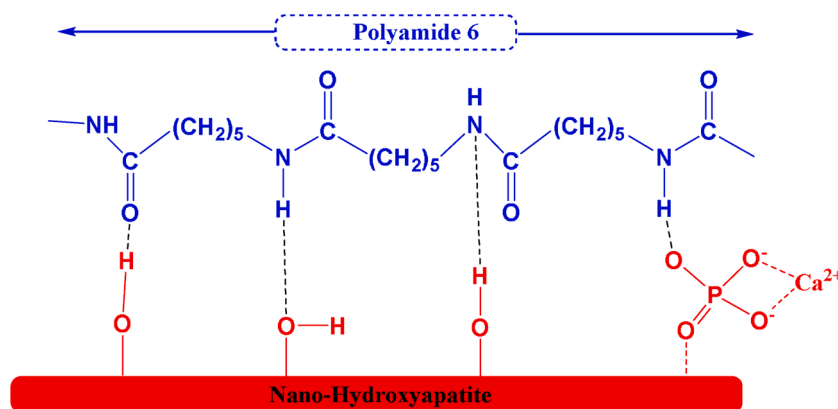
The suspension was aged overnight at room temperature. The precipitate was collected by centrifugation, carefully washed through several rinsing steps using demineralized water. Finally, the material was dried at 80 °C for 12 h, before grinding to a powdered form.

2.2.2. Synthesis of hybrid PA6/n-HAp

The hybrid material was prepared by melt compounding [61–64], using a Haake twin-screw extruder (Haake, PolyLab QC, Thermo Scientific, Waltham, MA, USA). The hydroxyapatite was dried overnight (at 80 °C) and stored in sealed desiccator prior to be incorporated into polyamide 6; it is important to remove any moisture from the mineral charge. Similarly, polyamide 6 chips were dried at 90 °C under vacuum for 24 h to remove adsorbed water. The melt-compounder (extruder) was operated at fixed rotational screw speed of 90 rpm, in the temperature range 250–255 °C. Under these conditions, the raw material can be melt and homogeneously mixed. Hydroxyapatite was incorporated at a mass dosage of 20 % w/w. The composite was extruded through a ribbon die into a cooling demineralized water bath and pelletized. The pellets were finally dried at 80 °C under vacuum for 24 h and grinded to a powdered form. The material, after intermediary storage in desiccator, was kept into sealed bottles. Scheme 1 shows the tentative mechanism describing the interaction mode between n-HAp and PA6.

2.3. Characterization of materials

The textural properties were recorded on a Quantachrome BET surface analyzer (Nova 3200 Quantachrome Instruments, Boynton Beach, FL, USA), operated with NovaWin software (v. 11.03) for data treatment. The samples were initially out-gassed under vacuum (10⁻⁴ Torr) at 150 °C for 3 h. The BJH method was used for calculating the pore volume and pore size, while the specific surface area was deduced from multipoint BET method. The X-ray diffraction patterns were acquired using an Empyrean diffractometer (Malvern Panalytical, Malvern, UK) and the Cu K_α wavelength (i.e., 1.54060 Å; generator setup: 30 mA; 45 kV). The morphology of nano-hydroxyapatite (n-HAp) was characterized by TEM analysis using a JEOL JEM-2100 electronic microscope (JEOL, Ltd., Tokyo, Japan) at an accelerating voltage of 120 kV. Fourier-transform infrared spectra were obtained using a Spectrum Two spectrometer (PerkinElmer, Waltham, MA, USA) equipped with an ATR sample base plate Diamond. Scanning electron microscopy was performed using a QUANTA FEG250 SEM (HV: 30 kV) (FEI Company, ThermoFisher Scientific, Waltham, MA, USA) equipped with a semi-quantitative energy dispersive X-ray analyzer (integrated to QUANTA FEG250 SEM). The characterization of hybrid material was carried out on a DSM 962 SEM (Carl Zeiss Ltd., Cambridge, UK with an integrated EDX analyzer). Zetasizer analysis was performed using a Nano Series Zeta (Nano-ZS Malvern Instruments Ltd., Malvern, UK) for analysis of particle size and zeta potential. The pH-drift method [65] was used for quantifying the pH_{PZC} of the materials. A fixed amount of sorbent (i.e., 100 mg) was distributed in a series of flasks (25 mL aqueous solutions,



Scheme 1. Tentative mechanism for the linkage of n-HAp with PA6 (H-bonding).

containing 0.01 M NaCl as the background salt, and with different initial values of pH, in the range 2–10). After 24 h of agitation, the final pH (pH_{eq}) was measured and compared to initial pH value (pH_0). The pH_{PZC} was approached by the pH value corresponding to $\text{pH}_0 = \text{pH}_{\text{eq}}$.

2.4. Sorption studies

2.4.1. Synthetic solutions

The sorption performances for U(VI) and REE(III)s from synthetic solutions are compared for raw PA6 sorbent and PA6/n-HAp composite. Sorption experiments were performed in batch mode. A fixed amount of sorbent (m, g) was mixed with a fixed volume (V, L) of metal-containing solution for a fixed contact time (i.e., 24 h) at room temperature (i.e., 25 ± 2 °C). The pH was not controlled during sorption experiments; however, the final pH value was systematically recorded using a Cyber Scan pH 6000 pH-meter (Eutech Instruments, Nijkerk, Netherlands). After contact, the solutions were separated and the residual metal concentration (C_{eq} , mmol L^{-1}) was evaluated by ICP-AES (inductively-coupled plasma atomic emission spectrometer, Activa M, Horiba-Jobin Yvon, Longjumeau, France). The sorption experiments were duplicated and the average value is calculated and used for sorption quantification; deviation did not exceed 5%. Annex A shows some example of the good reproducibility in sorption performances (for the study of the effect of sorbent dosage and uptake kinetics, Figs. A1 and A2, respectively).

For the study of pH effect (mono-component solutions), the initial metal concentration (C_0 , mg L^{-1} or mmol L^{-1}) was set to $\sim 50 \text{ mg L}^{-1}$ ($0.2 \text{ mmol U L}^{-1}$, $0.36 \text{ mmol Nd L}^{-1}$ or $0.30 \text{ mmol Er L}^{-1}$); the sorbent dosage (SD) was 1 g L^{-1} . For the other studies, the initial pH was set to 2.04 ± 0.3 and experiments were performed in multi-component solutions (C_0 : 50 mg L^{-1} of each metal ions). While investigating the effect of sorbent dosage, SD was varied between 0.25 and 2 g L^{-1} . For the study of sorption isotherms, the concentration of metal ions, C_0 , was varied between 30 and 300 mg L^{-1} of each metal ions. The residual concentrations were used for the determination of the sorption capacity (q_{eq} , mmol g^{-1}) using the mass-balance equation: $q_{\text{eq}} = (C_0 - C_{\text{eq}}) \times V / m$, and the sorption efficiency (%). Metal desorption was also carried out in batch systems using roughly the same experimental conditions (i.e., SD: 1 g L^{-1} ; room temperature; contact time: 24 h) by contact of the metal-loaded sorbent with a fixed volume of eluent (nitric acid, hydrochloric acid or sulfuric acid) at three levels of concentrations (0.1 M, 0.5 M and 1 M). After completion, the residual concentration in the filtrate was analyzed for evaluating the desorption efficiency.

The recycling of the sorbent (testing of sorption and desorption efficiencies) for 5 successive cycles was investigated by loading PA6/n-HAp with a ternary metal solution (at pH 2.03, containing 50 mg L^{-1} of U(VI), Nd(III) and Er(III)). The sorbent dosage was set to 1 g L^{-1} and the contact time was 24 h. The desorption of metal ions was carried out using again a sorbent dosage of 1 g L^{-1} while the eluent was nitric acid;

the suspension was maintained under agitation for 24 h. Desorption steps were processed sequentially beginning with 0.1 M HNO_3 solutions for the elution of REEs, followed by 1 M HNO_3 solutions for the recovery of U(VI). The solutions were mixed and analyzed for determining the cumulative desorption of target metals.

Table S1 (see Supplementary Information) reports the conventional equations used for modelling sorption isotherms and uptake kinetics. The parameters of these models were obtained by non-linear fitting with the facilities of Mathematica® software. The quality and the comparison of the fits were analyzed by both the determination coefficients (R^2 , comparing calculated and experimental data) and the AIC (Akaike Information Criterion).

2.4.2. Tests on ore leachate

In order to evaluate the robustness of sorption properties in complex solutions, a geological sample collected in an Egyptian mining site (El Sella area, Southeastern desert, [66]) was submitted to a sulfuric acid leaching. Grinded uranium ore (particle size $\sim 74 \mu\text{m}$) was mixed with a 10 % (w/w) sulfuric acid solution for 4 h at 45 °C: the solid/liquid mass ratio was 1:2 [67]. Filtrated leachate, after adjusting the pH to 1.96 using NaOH, was used for testing the recovery of a series of metal ions by PA6/n-HAp. The sorbent dosage was set to 1 g L^{-1} ; the sorption experiment was carried out at room temperature for a contact time of 8 h. Global index for REEs was determined using the Arsenazo III spectrophotometric method [68]. The concentration of P_2O_5 was determined by the ammonium molybdate and ammonium metavanadate method [69]. The concentrations of other metal ions were determined by ICP-AES. Sulfate concentration was obtained according to APHA Method (4500- SO_4^{2-}) of the standard methods for the examination of water and wastewater [70].

3. Results and discussion

3.1. Characterization of n-HAp and PA6/n-HAp

3.1.1. Morphology and chemical composition – TEM, SEM and SEM-EDX analysis

Fig. S1 (see Supplementary Information) shows the TEM characterization of n-HAp particles. Though some aggregates can be identified, most of the particles can be classified in two groups: 6–16 nm and 30–40 nm. In any cases, most of these particles can be qualified as nanoparticles. The process selected for the synthesis of hydroxyapatite allows manufacturing nanoparticles and the mineral fraction will be called n-HAp. Fig. 1 shows SEM microphotographs at different magnitudes to illustrate the heterogeneity in size and shape of the different objects. The melt compounding produces a material containing a homogeneous continuous phase (PA6 and n-HAp matrix) embedding irregular larger objects that consist of PA6. Fig. S2 shows the SEM

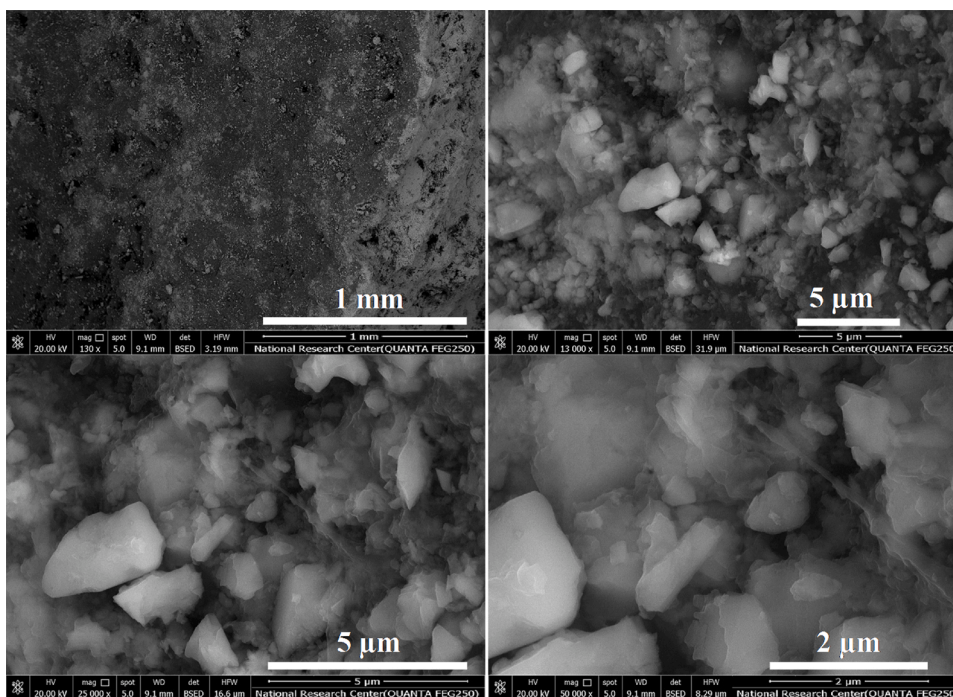


Fig. 1. SEM photomicrographs of PA6/n-HAp sorbent at different magnitudes.

observation of PA6, n-HAP and composite PA6/n-HAp together with their semi-quantitative EDX analysis. The stoichiometric ratios C/O and C/N are supposed to be close to 6 in PA6; here, the ratios are lower (in the range 4.41–4.68). The N/O ratio is close to 1 (consistently with PA6 formula). For n-HAP the porous structure is clearly appearing on the SEM microphotograph; the surface aspect is consistent with the pictures reported by Yan et al. [71]. Xia et al. [72] reported different structures associated with nanosheet formation in the synthesis of n-hydroxyapatite depending on the synthesis procedure. The semi-quantitative analysis shows that the O/P and O/Ca ratios are much lower (i.e., 2.07 and 1.59, respectively) than expected from theoretical formula $\text{Ca}_5(\text{PO}_4)_3(\text{OH})$ (i.e., 4.33 and 2.60, respectively). The Ca/P atomic ratio is close to 1.29; much lower than theoretical 1.67 ratio; Ni and Fox [73] reported even higher Ca/P atomic ratio (close to 2.1). This probably means that the synthesis does not produce pure hydroxyapatite and that several compounds based on calcium phosphate may coexist; this is consistent with further XRD characterizations (see below). In the case of the composite, the embedment of n-HAP in PA6 results in more compact surface (compared with n-HAP) with many micro particles deposited on the surface. The semi-quantitative analysis shows that the C/N atomic ratio (which can be considered a marker of PA6 compound) is close to 3.06, much lower than for raw PA6 (i.e., 4.68). While for raw n-HAP the Ca/P ratio was close to 1.29, in the composite the ratio increases to 2.84. This means that unexpectedly the melt compounding substantially modifies the chemical composition of the products incorporated in the composite. The relative fractions of P and Ca (markers of n-HAP) in the composite are about 8.13 to 3.69 lower than their atomic fractions in raw n-HAP. Based on these relative decreases the n-HAP content in the composite, hydroxyapatite represents between 12 and 27 % of PA6/n-HAP. This order of magnitude is consistent with the relative weight fractions of PA6 and n-HAP in the synthesis procedure (i.e., 80:20) and with the weight loss at 600 °C. Exposed overnight at a temperature of 600 °C in a vacuum muffle furnace, the weight loss (due to thermal degradation of PA6) represented 20.9 %.

3.1.2. Textural properties – BET analysis

Figs. S3 and S4 show the overview of the textural analysis of n-HAP, PA6 and PA6/n-HAP materials including BET surface area (S_{BET}) and

pore size distribution. The N_2 sorption-desorption curves are typical of Type II(b) sorption isotherm with a limited hysteresis phenomenon. For n-HAP, the S_{BET} is evaluated close to $61.6 \text{ m}^2 \text{ g}^{-1}$. This is consistent with the values reported by Yan et al. [71] for the synthesis of hydroxyapatite using distiller wastes, but much lower from the values cited by Xia et al. [72] in the case of hydroxyapatite produced from perforated shell powder (i.e., $188 \text{ m}^2 \text{ g}^{-1}$). Xia et al. characterized the effect of experimental procedures on the average pore size of different n-HAP materials from 6 to 69 nm; the present material shows an intermediary value for pore size (i.e., 36.4 nm). Similar trends were recorded for PA6/montmorillonite materials [42]. The pore volume of n-HAP being close to $0.33 \text{ cm}^3 \text{ g}^{-1}$ is much lower than the value reported by Xia et al. for their specific productions ($\sim 1.31 \text{ cm}^3 \text{ g}^{-1}$) but in the middle range of commercial n-HAP substrates ($0.15\text{--}0.96 \text{ cm}^3 \text{ g}^{-1}$) [72]. The PA6 material also presents a Type II(b) sorption isotherm with little hysteresis; the specific surface area is found close to $13.2 \text{ m}^2 \text{ g}^{-1}$; this value is consistent with the S_{BET} of PA6 nanofiber membranes (close to $15.8 \text{ m}^2 \text{ g}^{-1}$) [74]. The pore volume and the average pore size are close to $0.086 \text{ cm}^3 \text{ g}^{-1}$ and 2.2 nm, respectively; the material can be considered microporous; hindering the diffusion of metal ions into the sorbent. The incorporation of n-HAP has a limited impact on the textural properties of the composite: the S_{BET} is hardly increased to $14.7 \text{ m}^2 \text{ g}^{-1}$, the pore volume to $0.105 \text{ cm}^3 \text{ g}^{-1}$, and the average pore size to 1.6 nm. The coating of n-HAP porosity with PA6 during the melt compounding drastically reduces the textural properties of the mineral support.

3.1.3. Crystallographic properties – XRD analysis

The XRD diffraction patterns for the three materials are reported in Fig. S5. The patterns are weakly resolved with the presence of many peaks. The most representative are reported on the Table associated to Fig. S5. In the case of n-HAP, the main peaks (at 2θ : 6.60° , 8.3° and 15.92°) are associated with the crystal planes (100), (-110) and (-111) of octacalcium phosphate (reported to 4.7° , 9.0° and 15.8° by Xia et al. [72]). However, some peaks surrounding the characteristic peaks apparently indicate the presence of other phases such as calcium hydrophosphate (2θ : 11.6° and 23.4° , [72]) for example. Usually, PA6 XRD patterns are poorly resolved and characterized by two main peaks identified at 2θ : 20.4° and 24.1° [75]; here, the two main peaks are

detected at 2θ : 18.33° and 20.70°. They are surrounded by a series of peaks that make difficult the identification of crystal planes. As expected, PA6 is much less crystalline than n-HAp. The melt compounding of PA6 and n-HAp leads to XRD patterns that logically combine the contributions of the two compounds. As reported by Mehrabian and Nasr-Esfahani [75], the XRD pattern of the composite shows the superposition of the two patterns; slight shifts in the 2θ positions are observed (see Table in Fig. S5); this is probably due to the intercalation of PA6 in the planes of n-HAp.

3.1.4. Functionalization - FTIR analysis

The investigation of composites based on PA6 (produced by melt compounding of the polymer with fillers, charges and other polymers) provides a basis for the interpretation of the interactions between PA6 and n-HAp. Different mechanisms have been reported for explaining, for example, the interactions between hydroxyapatite, polyamide and polyethylene [64], including H-bonding (see Scheme 1). This mechanism was previously documented [58,76–79].

Fig. 2 reports the FTIR spectra of PA6, n-HAp, composite sorbent before and after the sorption of metal ions. The figure is focused on the 2000– 450 cm^{-1} wavenumber range because in the region 4000– 2000 cm^{-1} the differences are not marked enough to bring meaningful information. Table S2 reports the assignments of the main peaks for the different materials (and relevant references). Some peaks representative of phosphate groups (P=O stretching, P-O stretching) stretching are identified around 1090 cm^{-1} , 1026 cm^{-1} , 963 cm^{-1} , 601 cm^{-1} , 562 cm^{-1} and 471 cm^{-1} on n-HAp spectrum. Some of these peaks disappear (P—O stretching (ν_3 PO₄ stretching) at 1025.77 cm^{-1} , ν_1 PO₄ stretching at 962.61 cm^{-1} , and P-O stretching/ ν_4 PO₄ stretching or phosphate bending at 600.80 cm^{-1}) or are strongly shifted after incorporation with PA6 (to form PA6/n-HAp); for example P=O stretching vibration shifted from 1089.63 cm^{-1} to 1064.74 cm^{-1} . It is noteworthy that FTIR spectrum tends to indicate that carbonate may be present on the material as shown by the presence of CO₃ stretching signal (at 1419.65 cm^{-1}).

PA6 shows typical bands of amide groups, including C—O, C-N and C=O vibrations, at 1636.94 cm^{-1} (C-O and C-N stretching), 1535.00 cm^{-1} (C-N stretching or C-N bending), 1263.03 cm^{-1} (C-N stretching and /or C=O bending), 686.73 cm^{-1} (Amide V, band). After melt compounding, the sorbent shows the combination of PA6 and n-HAp spectra with some weak shifts of characteristic wavenumbers (see Table S2). It is noteworthy that some peaks disappear; for example at \sim 628.8 cm^{-1} and 600.8 cm^{-1} (corresponding to δ OH deformation and

P—O stretching/or phosphate bending vibrations, respectively): the interaction of PA6 with n-HAp affects the vibrational environment of these reactive groups. New peaks appear at \sim 893.7 cm^{-1} and \sim 801–173 cm^{-1} (probably associated to carbonate vibrations), \sim 522.8 cm^{-1} (not assigned or resulting from the shift (or the splitting) of the PO₄ stretching vibration initially detected at 561.7 cm^{-1}). A shoulder appears around 1597 cm^{-1} ; this means that the environment of amide groups is affected by the interaction with hydroxyapatite. In addition, two strong peaks also appears at \sim 1135.8 cm^{-1} and \sim 1738 cm^{-1} . The peak at 1738 cm^{-1} is generally associated with carboxyl groups; this may be explained by the linkage between hydroxyl group of hydroxyapatite and the carbonyl group of amide site of PA6 [64]. These observations confirm that different modes of interaction may contribute to the synthesis of the composite. Zuo et al. [64] identified hydrogen bonding and interactions between hydroxyl and phosphate from n-HAp and carboxyl and amine groups of PA6. Zhang et al. [76] reported the formation of hydrogen bonds between the amide group of PA66 and hydroxyl groups of hydroxyapatite in the synthesis of n-HA/PA66 composite.

The figure also reports the FTIR spectrum of PA6/n-HAp after metal sorption. Substantial changes are observed: the peaks at 1136 cm^{-1} , 1065 cm^{-1} , 999 cm^{-1} , 894 cm^{-1} and 783 cm^{-1} disappear. In addition, the weak shoulder appeared around 1600 cm^{-1} is weakened. These peaks were associated to the interactions between PA6 and n-HAp. This means that the amide groups (—NH, C=O) are the most reactive among the phosphate, carboxyl and amine groups present on the composite. It is noteworthy that the FTIR spectra of PA6 and PA6/n-HAp after metal sorption are very close; the main difference is observed at 1738 cm^{-1} (which is not reversed by metal binding). In addition, the peaks appearing at 1233 cm^{-1} and 1217 cm^{-1} (which are not present on both PA6 and PA6/n-HAp FTIR spectra) are representative of the specific interaction between metal ions and reactive groups at the surface of the composite material. The neighboring peak at 1263 cm^{-1} is assigned to amide groups; this could support the shift of the signal of a fraction of these reactive groups with metal binding.

3.1.5. Particle size and surface charge – Zetametry

Zetametric measurements allow characterizing both the size of the particles that were used for sorption tests (see Fig. S6) and the characterization of their zeta potential in water. Polyamide has a little higher negative charge than other materials. Dietz et al. [37] reported positive zeta potential for polyamide at pH 3, while the charge changes to negative at pH 4.5 and above. Janusz and Skwarek [80] characterized

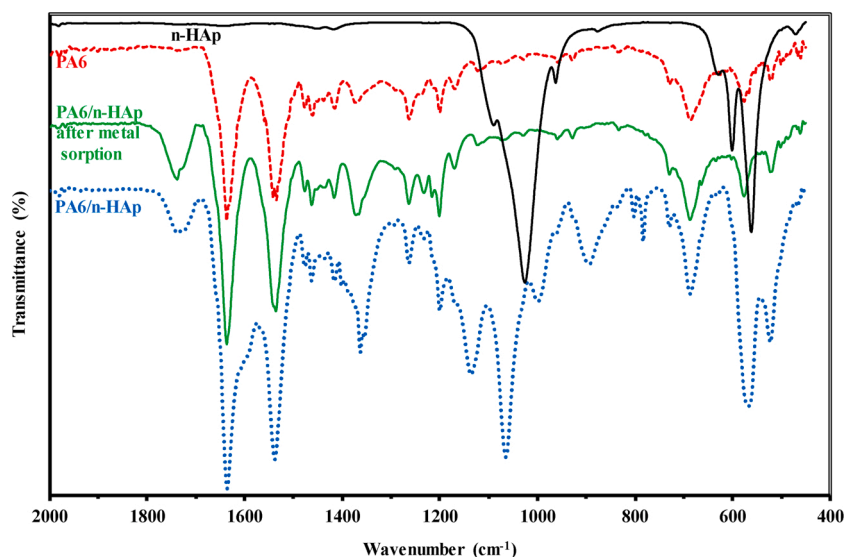


Fig. 2. FTIR spectra of n-HAp, PA6, PA6/n-HAp sorbent (before and after metal sorption) (wavenumber range 2000–450 cm^{-1}). (no significant difference in the range 4000–2000 cm^{-1} , except the absence of signals for mineral substrate, n-HAp).

hydroxyapatite with pH_{PZC} close to 7.5 while the pH_{IEP} was below 4. Ni and Fox [73] report a pH_{PZC} ~6.0–7.0 for hydroxyapatite. The melt compounding does not change significantly the overall negative charge of the composite: the net charge in demineralized water is closed to -15 mV, intermediary between those of n-HAp (i.e., -12 mV) and PA6 (i.e., -25 mV).

The analysis particle size of the three materials confirm that hydroxyapatite can be considered of nanometer-size (~ 54 nm), as well as the composite (~ 67 nm). On the opposite hand, PA6 raw material exhibit much larger particles, close to 602 nm. Obviously, the difference in size will induce a strong impact on mass transfer properties and uptake kinetics.

Debye–Scherrer equation was used to calculate the average crystallite size (L) of n-HAp, PA6 and PA6/n-HAp (Table S3) depending on XRD data (Fig. S5) [36]. The crystallite sizes obtained from Scherrer equation were less than those obtained from TEM and Zetasizer measurements.

The size obtained from Scherrer's formula is not necessarily the same as the particle size. This is the case for partly crystalline powders and aggregated powders made up of smaller primary particles [81]. Furthermore, powders are normally not monodisperse but consist of a size distribution. The polydispersity of nanopowders is not taken into account in Scherrer's formula [81].

Comparatively, particle size calculated from TEM and Zetasizer measurements will be more reliable. It seems that calculated crystallite size using Scherrer equation is less than the real size [82]. The point to be noted for the three materials is that a particle is composed of more individual crystallites. For example, crystallite size with 6.13 nm (determined from Scherrer equation) for n-HAp, and particle size ~ 30 – 40 nm (from TEM) means that crystallite size $<$ particle size and confirms that each particle is composed of many crystallites.

Fig. S7 shows the comparison of pH_{PZC} values for PA6 (i.e., 6.97) and PA6/n-HAp (i.e., 7.62) deduced from pH-drift titration. Apparently, these pH_{PZC} values are close to those of hydroxyapatite (see above; i.e., 6–7 to 7.5 depending on the synthesis routes). Consistently with the comparison of the zeta potential of the materials in suspension into water, the melt compounding hardly changes the range of pH_{PZC} values obtained with the pH-drift method (while comparing n-HAp, PA6 and the composite). Both PA6 and PA6/n-HAp materials are positively charged in acidic solutions. When the pH increases, the charge repulsion of metal cations with protonated surface groups progressively decreases. It is thus possible anticipating that with the increase of the pH the sorbents have a surface charge more compatible for the binding of metal cations.

3.2. Sorption properties

3.2.1. pH effect – Charge and functional affinity for metal binding

The effect of the pH is an important parameter in the design and optimization of a sorption process. In the case of metal ions, the pH influences not only the surface charge of the sorbent and its potential effect of attraction or repulsion of solute molecules, but also the speciation of the metal ions. Under the experimental conditions selected for this study, the speciation of rare earths is remains almost constant between pH 1 and pH 6: free REEs(III) represent the predominant species: Nd(III) fraction is higher than 99.4 %. In the case of Er(III) the fraction of free Er(III) decreases down to 97.7 % with increasing the pH up to pH 6 (free Er(III) is about 99.8 % at pH 5), while Er(III) also appears as $ErOH^{2+}$ traces. On the opposite hand, the aqueous chemistry of U(VI) is strongly changed by the pH (Fig. S8, using Visual MINTEQ, [83]). At pH 1, U(VI) is present as free uranyl (about 93.71 %, completed with UO_2Cl^+). At pH 3, the metal is only present under its free cation form (i.e., UO_2^{2+}). Above pH 3, the speciation diagram shows the increasing formation of hydrolyzed species, including UO_2OH^+ and polynuclear species (i.e., $(UO_2)_2(OH)_2^{2+}$, $(UO_2)_3(OH)_4^+$, $(UO_2)_4(OH)_7^+$, none of them exceeding 16 % and the most significant species: $(UO_2)_3(OH)_5^+$ represents up to 57.2 % at pH 5.02. It is noteworthy that above pH 5.03, the

software predicts the possible formation of insoluble uranium species. The zetametry characterization showed that in demineralized water the surface charge of the different sorbents is globally negative (in the range -25 – -12 mV). This means that the sorbent can bind positive species by electrostatic attraction at pH close to neutrality. In acidic conditions, the surface charge becomes positive (see the results of the pH-drift method).

Fig. 3 shows that for PA6, the sorption of REEs increases with the pH from 0.02 $mmol\ g^{-1}$ to 0.07 – 0.08 $mmol\ g^{-1}$, the sorption of Nd(III) being slightly higher than that of Er(III). The progressive deprotonation of sorbent surface favors the binding of metal cations. Rho et al. [84] reported a pH_{PZC} value close to 6.3 for polyamide nanofiltration membranes. This would suggest that the support remains positively charged on the whole range of pH tested for metal sorption; however, the overall charge progressively decreases making more favorable the sorption of Nd(III) and Er(III). The positive charge of both the sorbent and the metal ions means that their sorption proceeds through chelation on amide reactive groups (carbonyl and/or amine sites) rather than electrostatic attraction. In the case of uranyl sorption, the levels of uptake are very low, below 0.04 $mmol\ U\ g^{-1}$, reached at the optimum pH value (i.e., pH 3). Between pH 1 and 3 the progressive deprotonation reduces the charge repulsion of free uranyl species by charged PA6 surface. Above pH 3, despite a less defavorable surface charge the sorption tends to decrease; this is probably due to the progressive decrease in the relative fraction of free uranyl (Fig. S8) and the formation of hydrolyzed and polynuclear species of larger ionic size (which may limit the accessibility to internal sites). In the case of composite sorbent, the sorption properties are considerable increased. Under comparable experimental conditions, the sorption capacities for Nd(III) vary between 0.3 and 0.35 $mmol\ Nd\ g^{-1}$, with limited effect of pH (slightly higher around $pH_{eq}\ 3$) while for Er(III) the sorption capacity increases from 0.24 $mmol\ Er\ g^{-1}$ at pH 1 to 0.27 – 0.28 $mmol\ Er\ g^{-1}$ in the range pH_{eq} : 2–6. The pH has globally a limited effect on REE binding; the sorption being slightly higher around pH 3. For uranyl, the $q_e = f(pH)$ profile is similar to the profile observed for PA6. It is noteworthy that in acidic region, the sorption capacity slightly increases from $pH_{eq}\ 1$ to $pH_{eq}\ 3$ (from 0.14 to 0.17 $mmol\ U\ g^{-1}$) before strongly decreasing above pH 3 down to 0.3 $mmol\ U\ g^{-1}$. The composite shows sorption capacities 3–4 times higher than PA6 precursor.

For REE cations, the decrease in the overall surface charge of the sorbents favors their sorption by the reduction of repulsion effect and probably by chelation on $-NH$ and carbonyl/carboxyl groups (two reactive groups that have been affected by metal binding on FTIR spectra). For uranyl species, the sorption is also slightly increased with

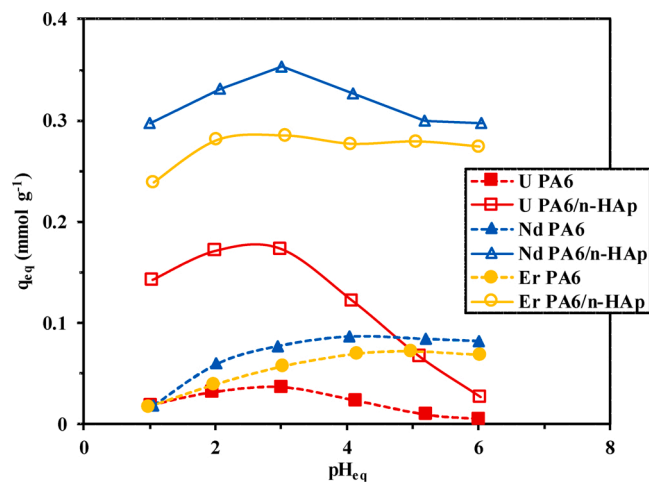


Fig. 3. Effect of equilibrium pH on the sorption of U(VI), Nd(III) and Er(III) using PA6 and PA6/n-HAp (mono-component solutions; Sorbent dosage, SD: $1\ g\ L^{-1}$; C_0 : $50\ mg\ L^{-1}$, $0.205\ mmol\ U\ L^{-1}$, $0.344\ mmol\ Nd\ L^{-1}$ or $0.298\ mmol\ Er\ L^{-1}$; room temperature; contact time: 24 h).

pH augmentation, until reaching $\text{pH}_{\text{eq}} \sim 3$ for the same reason (decrease in repulsion effects); however, at higher pH the formation of large size polynuclear hydrolyzed species limits the accessibility to internal reactive groups for uranyl species. The substantial increase in sorption performance between PA6 large particles and PA6/n-HAp is probably associated to the higher accessibility of reactive groups induced by the fractionation of the polymer microparticles (average particle size 602 nm) into small nanoparticles (i.e., 66 nm). On the other side, the uptake of a polynuclear uranyl species means that the binding of one molecule induces the sorption of several U atoms (2–4, see Fig. S8). The formation of polynuclear species enhances the surface sorption but may limit the diffusion and accessibility to internal sites.

Fig. S9a shows the \log_{10} plot of the distribution ratio ($D = q_{\text{eq}}/C_{\text{eq}}$, L g^{-1}) vs equilibrium pH. A breakdown of the slope of these curves is observed at pH close to 3: slope inversion for U(VI) and slope changes for REEs. The plots of the distribution curves show only linear sections with U(VI). The slope of the linear segments may be associated in ion-exchange processes to the stoichiometry of proton exchange with metal cations. Actually, the stoichiometric ratios for U(VI) on PA6/n-HAp are +0.74 and -0.76 before and after $\text{pH}_{\text{eq}} 3$, respectively. These values are “close” to 1; this is not consistent with the predominant uranyl species in this pH range (i.e., free UO_2^{2+}). Fig. S9b shows the comparison of equilibrium and initial pH values during metal sorption for both PA6 and PA6/n-HAp. The variation of pH is negligible, meaning that proton exchange is not the predominant binding mechanism.

3.2.2. Sorbent dosage – Optimization of sorbent dosage (SD)

Fig. 4 compares the effect of sorbent dosage on the sorption efficiency and the sorption capacity for the three metals using both PA6 and PA6/n-HAp. These experiments were performed at pH_0 2.04 using multi-element solutions. The speciation diagram is hardly affected by the ternary composition of the solution (not shown): free rare earths and free uranyl are largely predominating in the solution at pH 2–2.5. This figure clearly confirms the beneficial effect of the incorporation of n-HAp in the sorption performance of the composite. The sorption efficiency curves are almost superposed in the case of PA6 for the three metals: the sorption progressively increases with sorbent dosage from 5–8 % to 22–28 %. As expected, the increase of the SD results in a progressive decrease in sorption capacity (never exceeding $0.13 \text{ mmol metal g}^{-1}$ under selected experimental conditions). The same trends are observed with composite sorbent: the sorption efficiency increases with SD and tends to stabilize above $\text{SD} = 1 \text{ g L}^{-1}$ at least for REEs; indeed, the solution is almost exhausted in terms of Nd(III) and Er(III) concentrations. As usual, the sorption capacities decrease with increasing SD. In this case again, the affinity of the sorbent tends to decrease according to the series: $\text{Nd(III)} > \text{Er(III)} > \text{U(VI)}$. Obviously, this conclusion should be moderated since the mass concentration for each individual metal (i.e., 50 mg L^{-1}) means that molar concentration of U(VI) is lower than for the two REEs (i.e., $0.201 \text{ mmol U L}^{-1}$, $0.361 \text{ mmol Nd L}^{-1}$ and $0.302 \text{ mmol Er L}^{-1}$). The ranking of metal affinities will be analyzed through sorption isotherms (see Section 3.2.4.). Under selected experimental conditions (especially range of concentrations that are consistent with real industrial solutions and leachates) a good compromise for removal efficiency and sorption capacity would consist of $\text{SD}: 1 \text{ g L}^{-1}$.

3.2.3. Uptake kinetics – Mass transfer limitations

The uptake kinetics are compared in Fig. 5 for the different systems (sorbent and metal) from ternary solutions (containing $\sim 50 \text{ mg L}^{-1}$) at pH_0 2.04. This figure clearly illustrates again the beneficial effect of the incorporation of n-HAp in the composite sorbents not only in terms of sorption performance at equilibrium but also in terms of kinetic profiles, for the three metals. Under selected experimental conditions, $\text{SD}: 1 \text{ g L}^{-1}$, the sorption efficiency never exceeds 20 % with PA6 sorbent while metal removal varies between 96 % for Nd(III) and 80 % for U(VI) (90 % for Er(III)) in the case of PA6/n-HAp. Despite a higher density of amide groups in PA6 (compared with the composite) the metal binding is

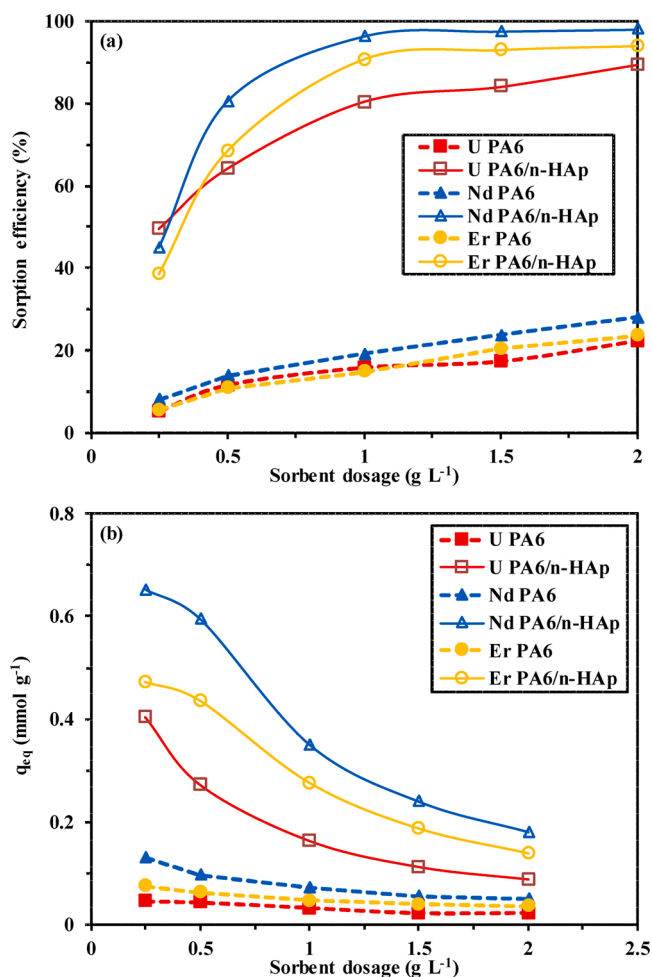


Fig. 4. Effect of sorbent dosage on U(VI), Nd(III) and Er(III) sorption efficiency (a) and sorption capacity (b) (multicomponent solutions; Sorbent dosage, SD: 0.25–2 g L⁻¹; C₀: 50 mg L⁻¹, 0.205 mmol U L⁻¹, 0.342 mmol Nd L⁻¹ or 0.297 mmol Er L⁻¹; pH₀: 2.04; pH_{eq}: 2.08 ± 0.02; room temperature; contact time: 24 h).

decreased. This is a clear confirmation that all the reactive groups are not available in PA6 microparticles, while the composite offers more available and accessible sorption sites. In terms of kinetics, the shape of the profiles also confirm that the initial slopes for PA6 sorbent are much lower than are those of composite materials, regardless of the metal. As an example, in the case of PA6/n-HAp about 88 % of total sorption occurs within the first two hours of contact; on the opposite hand, for the same contact time sorption represents only 58 % for REEs and 66 % for U(VI) in the case of PA6.

The kinetic profiles have been fitted with the PFORE (pseudo-first order rate equation), the PSORE (pseudo-second order rate equation) and the RIDE (resistance to intraparticle diffusion, the so-called Crank equation) (Table S1a). Table 1 reports the parameters of these models for the different systems while the solid lines in Fig. 5 shows the respective fittings. The comparison of R² and AIC values does not allow clearly stating the preferential model for fitting experimental profiles: the selection depends on the metal and the sorbent. In the case of U(VI), the RIDE model systematically gives the best fitting accuracy. In the case of REEs and PA6, the PFORE allows getting higher values for both R² and AIC while for PA6/n-HAp the PSORE is more efficient for Nd(III); for Er(III), both the PSORE and the RIDE give good fits. Cheira et al. concluded that U(VI) sorption onto PA6 and PA6/montmorillonite is preferentially described by the PSORE [42]. Comparing experimental values of the sorption capacity at equilibrium (q_{eq}) with calculated values (q_{eq,1} or

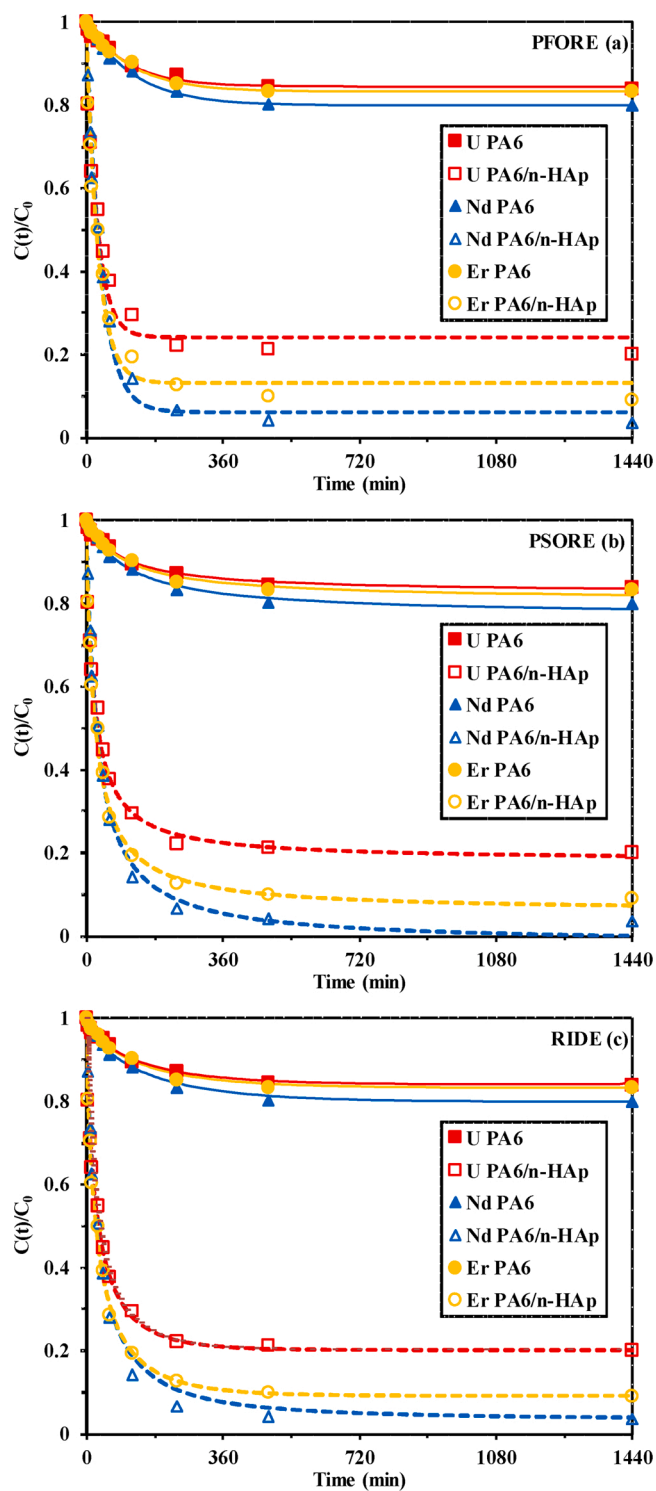


Fig. 5. Uptake kinetics for the sorption of U(VI), Nd(III) and Er(III) using PA6 and PA6/n-HAp sorbents – Modeling with the PFORE (a), PSORE (b) and the RIDE (c) equations (multicomponent solutions; Sorbent dosage, SD: 1 g L^{-1} ; C_0 : 50 mg L^{-1} , $0.205 \text{ mmol U L}^{-1}$, $0.342 \text{ mmol Nd L}^{-1}$ or $0.297 \text{ mmol Er L}^{-1}$; room temperature; pH_0 : 2.04; pH_{eq} : 2.06).

$q_{\text{eq},2}$) shows that the PFORE gives a better approximation of experimental values. Taking into account the small size of the sorbent particles, the time required to reach equilibrium (i.e., several hours) clearly mean that the mass transfer is controlled by diffusion mechanisms, and more specifically the resistance to intraparticle diffusion. Therefore, the effective diffusivity coefficients (i.e., D_e) are very low (ranging between

Table 1

Uptake kinetics for U(VI), Nd(III) and Er(III) sorption onto PA6 and PA6/n-HAp sorbents from ternary solutions – Modeling with the PFORE, the PSORE and the RIDE.

Model	Sorbent Metal	PA6			PA6/n-HAp		
		U(VI)	Nd (III)	Er (III)	U(VI)	Nd (III)	Er (III)
Exper.	q_{eq} (mmol g^{-1})	0.032	0.073	0.051	0.160	0.349	0.274
	$q_{\text{eq},1}$ (mmol g^{-1})	0.031	0.072	0.051	0.152	0.339	0.262
PFORE	$k_1 \times 10^2$ (min^{-1})	0.94	0.81	0.85	3.45	2.61	3.17
	R^2	0.986	0.997	0.995	0.975	0.991	0.982
	AIC	-101	-116	-114	-62	-69	-63
	$q_{\text{eq},2}$ (mmol g^{-1})	0.035	0.083	0.058	0.164	0.368	0.284
PSORE	$k_2 \times 10^1$ ($\text{g mmol}^{-1} \text{min}^{-1}$)	3.19	1.11	1.72	3.06	0.97	1.59
	R^2	0.987	0.992	0.988	0.995	0.995	0.996
	AIC	-105	-104	-105	-82	-77	-81
	$D_e \times 10^{17}$ ($\text{m}^2 \text{min}^{-1}$)	13.4	11.6	12.9	0.209	0.034	0.097
RIDE	R^2	0.991	0.994	0.994	0.998	0.993	0.993
	AIC	-113	104	-110	-90	-71	-84

$1.34 \times 10^{-16} \text{ m}^2 \text{min}^{-1}$ and $3.4 \times 10^{-19} \text{ m}^2 \text{min}^{-1}$). This means several orders of magnitude than the values reported for the self-diffusivity of metal ions in water [85] (around $4.8 \times 10^{-8} \text{ m}^2 \text{min}^{-1}$ for U(VI), $3.45 \times 10^{-8} \text{ m}^2 \text{min}^{-1}$ for Nd(III), and $3.48 \times 10^{-8} \text{ m}^2 \text{min}^{-1}$ for Er(III)). In the study of Er(III) diffusion in porous sol-gel glass, Koone et al. [86] reported the correlation between diffusivity coefficients and parameters such as REE ionic size and hydration number. Herein, the relatively higher diffusivity coefficient for Er(III) compared with Nd(III) is consistent with this explanation. The diffusion is controlled by size of ionic species in relation with the size of pores; this effect is highlighted, in the case of non-adsorbing conditions, by the so-called Renkin equation [87]. The BET analysis showed that the incorporation of n-HAp allows slightly increasing the average pore size (from 2.2 to 2.6 nm); this is not enough for making substantial differences in the mass transfer of REEs(III) and U(VI). Under selected experimental conditions (i.e., pH 2.44) uranyl (in its hydrated form) is present as free divalent cation with an ionic radius close to 1.08 \AA intermediary between the values of Nd (III) (i.e., 1.16 \AA) and Er(III) (i.e., 1.01 \AA) [88]. However, the effective diffusivity in the sorbents is higher for uranyl than for REEs, especially for PA6/n-HAp. This is consistent with the values of the apparent rate coefficients (both k_1 and k_2 parameters), which systematically follow the sequence: U(VI) > Er(III) > Nd(III). Divalent uranyl cation ($\text{UO}_2(\text{H}_2\text{O})_2^{2+}$), with lower hydration number [88], appears to be more readily transferred and sorbed in the sorbents than trivalent rare earth cations (as $\text{Nd}(\text{H}_2\text{O})_9^{3+}$ and $\text{Er}(\text{H}_2\text{O})_9^{3+}$).

Low specific surface area PA6, with small pores, shows weak mass transfer properties requiring long contact time for reaching equilibrium. These limitations to mass transfer reduce the accessibility to internal reactive groups. This means that sorbent particles should be decreased to improve mass transfer and reactivity. This is also achieved by the melt compounding of PA6 with nano particles of hydroxyapatite, as appearing in the comparison of the kinetic profiles.

3.2.4. Sorption isotherms – equilibrium performance

Another important criterion for evaluating the properties of the sorbent consists of the sorption isotherm that plots the distribution of the solute at equilibrium between the liquid and solid phase at a given pH and temperature for increasing metal concentrations. The sorption isotherm provides two important insights: (a) the maximum sorption capacity achieved at saturation of the sorbent (the plateau appearing in Fig. 6), and (b) the affinity of the sorbent for the solute (approached by

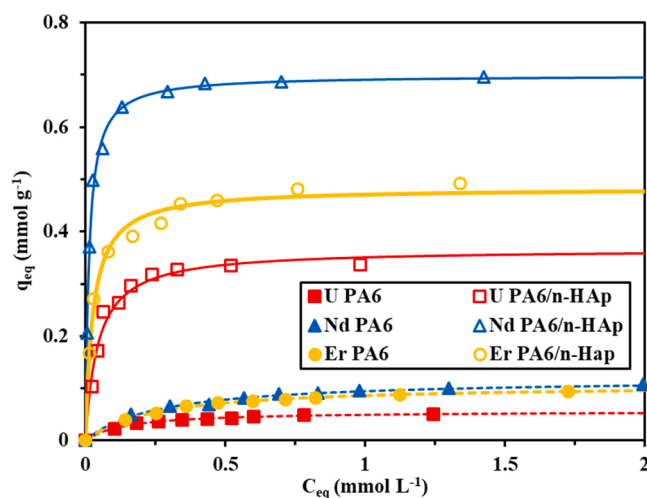


Fig. 6. U(VI), Nd(III) and Er(III) sorption isotherms using PA6 and PA6/n-HAp (multicomponent solutions; Sorbent dosage, SD: 1 g L⁻¹; C₀: 30-300 mg L⁻¹, 0.12-1.2 mmol U L⁻¹, 0.13-1.30 mmol Nd L⁻¹ or 0.182-1.82 mmol Er L⁻¹; pH₀: 2.04; pH_{eq}: 2.04 ± 0.03; room temperature; contact time: 24 h; solid lines: modeling with the Langmuir equation and parameters summarized in Table 2).

the initial slope of the curves in Fig. 6). The comparison of U(VI), Er(III) and Nd(III) sorption isotherms for PA6 and PA6/n-HAp confirms the drastic improvement of sorption performance while incorporating n-HAp: the maximum sorption capacities are increased 6.6, 6.5 and 5.2 times for U(VI), Nd(III) and Er(III), respectively. In addition, the initial slope of the isotherms is higher for composite material. Again, the sorbents show preference for metal ions according to the series: Nd(III) > Er(III) > U(VI). Table 2 compares the fits of sorption isotherms (performed in ternary solutions) with the Langmuir, the Freundlich and the Sips equations (Table S1b). The asymptotic shape of the sorption isotherm corresponds to the saturation of the sorbent, which, in turn, explains that the Freundlich equation (a power-type function, supposed to describe multi-layer sorption with heterogeneous sorption energies) is not appropriate for describing metal sorption on both PA6 and PA6/n-HAp. The Sips equation (Langmuir-Freundlich concept) introduces a third-adjustable parameter, which is supposed to improve the quality of curve fitting; this is confirmed by the higher R² values. However, the AIC takes into account the effect of number of adjustable parameters and shows that, in most cases, the Langmuir equation better describes experimental profiles (the unique exception concerns U(VI) sorption onto PA6/n-HAp, which is better fitted by the Sips equation). The Langmuir equation supposes the sorption to occur as a monolayer, with no interactions between sorbed molecules and homogeneous sorption energies. The sorption capacities at saturation of monolayer (i.e., q_{m,L})

are roughly consistent (slightly overestimated, except for Er(III) onto PA6/n-HAp) with the experimental values of maximum sorption capacities. The affinity coefficients (i.e., b_L) are substantially increased for PA6/n-HAp compared with PA6: by 3.3 for U(VI), 9.5 for Er(III) and up to 20.5 for Nd(III). The ranking of affinity coefficients follows the same order than maximum sorption capacities: Nd(III) > Er(III) > U(VI) for PA6/n-HAp (contrary to PA6: U(VI) > Er(III) ~ Nd(III)). Uranyl and rare earths are classified as hard acids according to the Pearson rules [89]; they are supposed to be preferentially bound to hard bases (bearing O- and N-donor ligands, for example as in PA6-based materials). Trivalent cations are usually considered having a more pronounced hard behavior; the hardness being also modulated by the ionic size of the metal. According to these rules neodymium is the harder of the three metals, which may explain its higher affinity for PA6/n-HAp; for the ranking of Er(III) and U(VI), apparently the charge criterion is more important than the ion size impact. The covalent index (CI: χ^2/r , with χ the Pauling electronegativity and r the covalent radius) and the ionic index (II: Z^2/r , with Z the ion formal charge) can be used for ranking the three metals ions. The order of affinity and sorption of the metal ions for PA/n-HAp follows the reciprocal trend of the CI: Nd(III) (0.69) < Er(III) (0.87) < U(VI) (1.58); contrary to the II that does not show any correlation in trends: U(VI) (2.19) < Nd(III) (4.79) < Er(III) (5.08). Apparently, the covalent nature is more important than the ionic criterion for explaining the affinity of the sorbent for selected metal ions.

Table S4 summarizes sorption properties for Nd(III), Er(III) and U(VI) for alternative sorbents. The comparison with PA6/n-HAp shows that several sorbents are more efficient than the present composites. However, it is noteworthy that these most efficient sorbents are generally designed for the sorption of target metals at less acidic pH values. Considering the sorption properties for acidic solutions (consistent with the application to metal recovery from acidic leachates) PA6/n-HAp is part of the most efficient materials. Typically, for U(VI) the maximum sorption capacity is comparable with those of commercial resins [21]. For REEs, the composite exhibits very attractive sorption properties at pH 2.44; comparable to most of the sorbents reported. The alternative sorbents having higher sorption capacities require higher pH values for reaching outstanding sorption capacities.

3.2.5. Metal desorption – Selection of eluent

Designing a new sorbent and a sorption process also requires optimizing the metal desorption for valorizing the metal, concentrating the hazardous contaminant and for recycling the sorbent. The study of metal desorption was performed playing with different acidic eluents at different concentrations. Fig. 7 compares desorption performances for these eluents for PA6/n-HAp after metal loading (in ternary solutions). The sorbent contained initially the following metal loadings: 0.36 mmol Nd g⁻¹, 0.28 mmol Er g⁻¹ and 0.16 mmol U g⁻¹. As expected, the two rare earths have very comparable responses to type and concentration of

Table 2
U(VI), Nd(III) and Er(III) sorption isotherms using n-HAp and PA6/nHAp sorbents – Modeling with Langmuir, Freundlich and Sips equations.

Model	Parameter	PA6			PA6/n-HAp		
		U(VI)	Nd(III)	Er(III)	U(VI)	Nd(III)	Er(III)
Experim.	q _m (mmol g ⁻¹)	0.051	0.107	0.094	0.336	0.697	0.492
	q _{m,L} (mmol g ⁻¹)	0.056	0.120	0.107	0.367	0.700	0.483
Langmuir	b _L (L mmol ⁻¹)	6.85	3.83	4.10	22.5	78.4	37.9
	R ²	0.995	0.994	0.998	0.984	0.996	0.991
	AIC	-133	-116	-127	-80	-80	-79
	k _F	0.051	0.092	0.085	0.385	0.742	0.510
Freundlich	n	3.68	3.48	3.32	4.76	7.03	5.64
	R ²	0.981	0.986	0.977	0.897	0.907	0.956
	AIC	-119	-107	-105	62	-48	-63
	q _{m,S} (mmol g ⁻¹)	0.058	0.135	0.105	0.340	0.697	0.517
Sips	b _S (L mmol ⁻¹)	5.80	2.36	4.40	103.2	93.2	14.2
	n _S	1.07	1.27	0.969	0.690	0.963	1.32
	R ²	0.995	0.996	0.998	0.993	0.997	0.995
	AIC	-129	-115	-123	-84	-76	-71

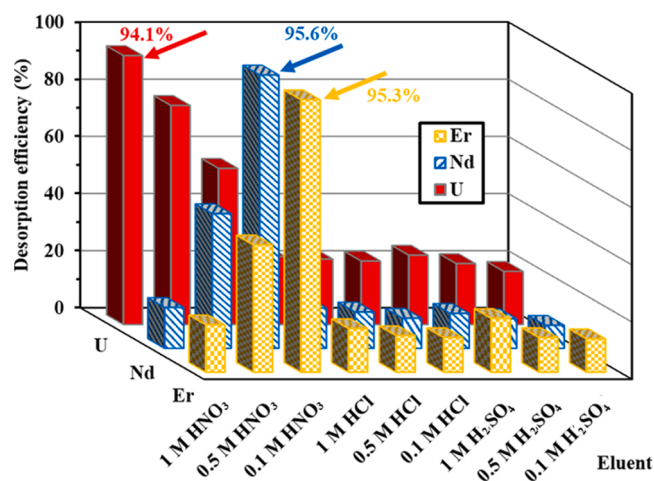


Fig. 7. Effect of the eluent (type and concentration) on U(VI), Nd(III) and Er(III) desorption from metal-loaded PA6/n-HAP sorbent (SD for both metal loading and desorption test: 1 g L^{-1} ; room temperature, contact time: 24 h; multicomponent solutions for metal loading at C_0 : 50 mg L^{-1} at pH_0 : 2.04).

acids in terms of desorption efficiency: the most efficient eluent consists of 0.1 M HNO_3 solution and the elution yield reaches 95.3–95.6 %. A higher nitric acid concentration is required for the elution of U(VI): uranyl desorption reaches 94.1 % for 1 M HNO_3 solution. For separating the different metals, the suggested sequence would consist of: (a) first desorption of U(VI) with 1 M HNO_3 solution (Nd and Er elution remains below 17 %), followed by (b) the desorption of REEs using 0.1 M HNO_3 solution. The reverse sequence appears inappropriate since the 0.1 M HNO_3 solution removes about 55 % of bound uranyl, simultaneously to 95 % of REEs.

The elution of the metal-loaded sorbent with 0.1 M HNO_3 solution is supposed to produce an eluate with enriched REE concentration containing much lower concentrations of uranyl. The separation of REEs from U(VI) would be readily operated using oxalic acid for the selective precipitation (and valorization) of REEs [90].

3.2.6. Sorbent recycling

Table 3 reports the performances of U(VI), Nd(III) and Er(III) sorption and desorption for PA6/n-HAP during 5 successive sorption/desorption cycles. The desorption efficiency remains remarkably stable for the 5 cycles: around $94.5 \pm 0.5 \%$, $95.1 \pm 1.0 \%$ and $94.8 \pm 0.6 \%$ for U(VI), Nd(III) and Er(III), respectively. The three metals are similarly desorbed using 1 M HNO_3 for uranyl and 0.1 M HNO_3 for REEs. The differences are more marked in the case of sorption performance: U(VI) (i.e., $75.9 \pm 4.1 \%$) < Er(III) (i.e., $88.0 \pm 2.5 \%$) < Nd(III) (i.e., $94.9 \pm 1.9 \%$). The sorption of REEs on PA6/n-HAP is more robust than the recovery of U(VI): the sorption performance remain relatively stable for the first 4 cycles and slightly decreases at the fifth; contrary to U(VI) uptake that continuously decreases for the 5 cycles. However, it is worth noting that the sorption loss is limited to 14 % for U(VI), 8 % for Er(III) and only 5 % for Nd(III) at the last cycle. It is noteworthy that the sorbent loss during the successive sorption and desorption steps was negligible (less than 5 %): the material is stable. This is consistent with the recycling performances reported for many alternative sorbents. This

Table 3

Sorption (S) and desorption (D) efficiencies (%) for U(VI), Nd(III) and Er(III) recovery from ternary solutions over five successive cycles.

Cycle	Run #1		Run #2		Run #3		Run #4		Run #5	
	S	D	S	D	S	D	S	D	S	D
U(VI)	80.3	94.4	79.6	94.9	76.9	94.1	73.6	95.1	69.2	93.9
Nd(III)	96.4	95.8	96.1	96.1	95.7	95.3	95.2	94.9	91.3	93.2
Er(III)	90.2	95.1	89.7	95.2	88.7	94.7	88.2	95.2	83.3	93.6

also demonstrates the feasibility of sorbent recycling.

3.2.7. Application to metal recovery from acid leachate of ore – Effect of solution complexity

The working solution for the simulation of industrial application was obtained from the leaching of El-Sella uranium ore using sulfuric acid solution. Ore was grinded and the fraction of particle size lower than $74 \mu\text{m}$ (200 Mesh) was collected. A 10 % w/w sulfuric acid solution was used for leaching tests with a solid/liquid mass ratio of 1:2, a stirring time of 240 min (stirring speed: 300 rpm), at a temperature of $45 \text{ }^\circ\text{C}$ [67]. The composition of leachate is summarized in Table 4, together with the residual concentrations after sorption test using PA6/n-HAP. The leachates contain three major metal elements: aluminum, iron and sodium. Iron concentration is slightly decreased after sorption while for aluminum and sodium the loss of metal ions is negligible. Phosphate and sulfate content are not affected by the contact with the sorbent. Other significant constituents are uranium and REEs. The global index of REEs (measured by the spectrophotometric method) shows that the sorption process is highly efficient: the desorption yield reaches 94 %, the sorption capacity corresponds to $90.2 \text{ mg REE}_{\text{eq}} \text{ g}^{-1}$. It is noteworthy that the distribution ratio (i.e., D) is higher than 15, as a clear confirmation of the affinity of the sorbent for REEs in complex solutions. The sorption capacity for U(VI) does not exceed $0.315 \text{ mmol U g}^{-1}$ (i.e., 75 mg g^{-1}). This value is close to the maximum sorption capacity found with ternary pure solutions (Table 2); the loss in sorption capacity does not exceed 7 %. Despite the complexity of the leachate (high ionic strength), the sorbent maintains good sorption performance for U(VI). The high relative concentration of the metal in the leachate does not allow reaching high distribution ratio (close to 0.37). It is noteworthy that thorium (frequently associated with uranium) is strongly adsorbed onto PA6/n-HAP: sorption efficiency exceeds 86 % and the distribution ratio reaches up to 6.5. The similarity in chemical properties between Th (IV) and U(VI) can explain the good uptake of thorium. Other base metals (such as copper and nickel) are also present in the leachate at concentrations around $12\text{--}13 \text{ mg L}^{-1}$; their removal is rather limited (efficiency in the range 16–29 %) and the sorption capacities range between 0.03 and 0.06 mmol g^{-1} . This means that the sorbent has a

Table 4

Recovery of REEs and uranium from acidic leachate of Egyptian ore (El Sella mining area) by sorption onto PA6/n-HAP.

Compd.	C_0 (mg L^{-1})	C_{eq} (mg L^{-1})	Sorption efficiency (%)	Sorption capacity (mg g^{-1})	Sorption capacity ($\mu\text{mol g}^{-1}$)	Distribution ratio, D (L g^{-1})
Fe(III)	1272	1200	5.7	72	1289.17	0.06
S(VI)	1341	1339	0.15	2	62.5	Negl
P(V)	76	75	1.3	1	32.29	0.01
Al(III)	2900	2898	0.07	2	74.13	Negl
Na(I)	980	979	0.1	1	43.48	Negl
Cu(II)	13.0	9.2	29.2	3.8	59.8	0.413
Ni(II)	12.0	10.1	15.8	1.9	32.4	0.188
Th(IV)	6.0	0.8	86.7	5.2	22.4	6.5
U(VI)	280	205	26.8	75	315.1	0.366
REEs ^a	96	5.8	94.0	90.2	–	15.6

^a global index, analyzed by spectrophotometry; Negl: negligible (≤ 0.001). (pH_0 : 1.96; contact time: 480 min; room temperature; SD: 1 g L^{-1}).

marked preference for target metals: REEs and U family metal ions against base metals.

This preliminary test confirms that PA6/n-HAp has a broad affinity for metal ions (binding REEs, U and analogues, base metals) but even in complex solutions (containing aluminum, iron, sodium, phosphate and sulfate in large concentrations) the sorbent has a marked preference for U, Th and REEs over base metals, and alkaline metals.

4. Conclusion

The incorporation of a small fraction of hydroxyapatite nanoparticles (about 20 %, w/w) into PA6, via melt compounding, contributes to significantly improving the sorption properties of the polymer for the sorption of a series of metal cations (such as uranyl and rare earth elements) in acidic solutions. Hydrogen bonding between hydroxyl groups of hydroxyapatite and amide groups of the polymer is responsible of the stability of composite material. The composite material having a nanometer size (close to 67 nm, vs. 602 nm for PA6) increases the availability and accessibility of reactive groups (-C = O and -NH groups) compared with single PA6. The optimum pH for the sorption of uranium and REEs (Nd for light REEs and Er for heavy REEs) is found close to 2–2.5. The binding mechanism is attributed to complexation of free cations by amide groups. The preference in sorption (Nd(III) > Er(III) > U(VI)) appears to be correlated to the covalent rather than ionic character of these metal ions. Maximum sorption capacities (0.336 mmol U g⁻¹, 0.492 mmol Er g⁻¹, and 0.697 mmol Nd g⁻¹) are significantly improved (by 5–7 times) compared with PA6. The sorption isotherms are finely fitted by the Langmuir equation. The uptake kinetics are controlled by the resistance to intraparticle diffusion and the profiles are fitted by the pseudo-second order rate equation.

Metal desorption is highly effective (higher than 94 %) using nitric acid. The sorbent also show good recycling properties. The sorbent is highly efficient for the recovery of U(VI), Th(IV) and REE(III)s from complex solutions such as the sulfuric acid leachate of Egyptian ores collected from El Sella mining site.

It is noteworthy that the sorbent shows good sorption properties for U(VI) and REEs in acidic conditions compared with literature; about 88 % of total sorption occurs within 120 min of mixing. These results confirm that the composite PA6/n-HAp sorbent is a good candidate for the recovery of valuable metals, even in complex media (such as acidic leachates). In addition, this work confirms that the incorporation of a small fraction of hydroxyapatite nanoparticles into PA6 allows drastically improving the potential of these PA6-based materials.

CRedit authorship contribution statement

Taha F. Hassanein: Conceptualization, Methodology, Investigation, Writing - review & editing. **Ahmed M. Masoud:** Conceptualization, Methodology, Investigation, Writing - review & editing, Supervision. **Wael S. Mohamed:** Conceptualization, Methodology, Investigation, Writing - review & editing. **Mohamed H. Taha:** Conceptualization, Formal analysis, Writing - original draft. **Eric Guibal:** Data curation, Validation, Supervision, Writing - review & editing.

Declaration of Competing Interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

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Appendix A. Supplementary data

Supplementary material related to this article can be found, in the online version, at doi:<https://doi.org/10.1016/j.jece.2020.104731>.

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